

ESL-TR-81-46

PREDICTIVE MODEL FOR JET ENGINE TEST CELL OPACITY

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30 SEPTEMBER 1981

FINAL REPORT
1 JULY 1980 - 30 SEPTEMBER 1981



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REPORT DOCUMENTATION	READ INSTRUCTIONS BEFORE COMPLETING FORM		
. REPORT HUMBER	2. GOVT ACCESSION NO	. 3. RECIPIENT'S CATALOG NUMBER	
ESL-TR-81-46	AD-A117585	<u> </u>	
PREDICTIVE MODEL FOR JET ENGINE TEST CELL OPACITY		FINAL REPORT July 1 1980-Sept. 30, 198	
	S. PERFORMING ONG. REPORT NUMBER		
. AUTHOR(e)	8. CONTRACT OR GRANT NUMBER(*)		
DR. GORDON A. LEWANDOWSKI	FO 8635-80-C0222		
PERFORMING ORGANIZATION NAME AND ADDRESS	10. PROGRAM ELEMENT, PROJECT, TASK AREA & WORK UNIT NUMBERS		
New Jersey Institute of T 323 High Street Newark, NJ 07102	P.E. 62601 F JON: 1900-90-11		
AFESC/RDVS Tyndall AFB, Florida 32403		September 30, 1981	
		13. NUMBER OF PAGES 72	
4. MONITORING AGENCY NAME & ADDRESS(II dilleren	18. SECURITY CLASS. (of this report)		
		UNCLASSIFIED	
·	•	150. DECLASSIF: CATION/DOWN GRADING	

Approved for public release; distribution unlimited

17. DISTRIBUTION STATEMENT (of the obstract entered in Black 20, if different from Report)

18. SUPPLEMENTARY NOTES

Availability of this report is specified on verso of front cover.

19. KEY WORDS (Continue on reverse side if necessary and identify by block number)

Computer Program Jet Engine Test Cell Light Scattering

Test Cell Visibility

Opacity

20. ABSTRACT (Confinue on reverse side if necessary and identify by block number)

A computer program (written in FORTRAN for a CDC 6600) was developed to predict the plume opacity of jet engine test cells. The data input quired for the model includes: the particle density, concentation, and size distribution in the exhaust gas, and the effective stack diameter. Previous data obtained for J-57 engines were used to test the model, and the difference

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between the theoretical and measured transmittance was generally within one percent.

The program also predicts the theoretical effect of using electrostatic precipitators or venturi scrubbers to treat the exhaust emissions. These predictions indicate that control devices larger than the test cells would have to be installed to even achieve a minimal effect on the observed visibility.

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PREFACE

This report was prepared at the Department of Chemical Engineering, New Jersey Institute of Technology, 323 High Street, Newark, New Jersey 07102, under contract No. FO 8635-80-CO222 with the Air Force Engineering and Services Center, Tyndall Air Force Base, Florida 32403. Capt. D. Berlinrut managed the program for the Air Force Engineering and Services Center. The work was begun July 1, 1980 and completed September 30, 1981.

The author, Dr. Gordon A. Lewandowski, is indebted to the following individuals and organizations: Dr. W. Wong of New Jersey Institute of Technology for his valuable suggestions regarding stable generation of the complex Riccati-Bessel functions; Exxon Research & Engineering Co. (ERE) for release of their opacity computer program which was used to check the results of the program presented in this report; and S. Shaw of ERE for her efforts to obtain the release of their program and for guidance in its use.

This report has been reviewed by the Public Affairs Office and may be released to the National Technical Information Service (NTIS), where it will be available to the general public, including foreign nations.

This technical report has been reviewed and is approved for publication.

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SECTION I

INTRODUCTION

A generalized schematic of a jet engine test cell is shown in Figure 1. Generally, the width of a plume issuing from a test cell is approximated by the stack dimension. The stacks are usually square; however, they contain acoustical baffles which considerably reduce the open area. For the calculations made in this report, the plume width was assumed to be the square root of the net open stack area.

Dimensions can vary considerably, depending upon the particular cell design, but the principle of operation is always the same. An engine that has been repaired, or otherwise maintained, is placed in the cell to test it under flight conditions before being remounted on the aircraft. The engine is considered a mobile emission source which is governed by Federal rather than state regulations. However, the test cell is immobile, and on that basis a U.S. District Court upheld the right of the State of California to regulate test cell emissions (Reference 1) which occasionally violate state visibility requirements of Ringelmann 1 (20% opacity). Since the U.S. Air Force has a large number of test cells in California, this court ruling can have a significant impact on Air Force operations and capital expenditures.

In order to satisfy state regulations, there are three possible alternatives: (1) design smokeless engines and install them on all existing aircraft; (2) introduce fuel additives to minimize soot formation; (3) use particulate control devices to treat the test cell exhaust.

The first of these alternatives is already being pursued as a result of the military incentive to reduce visibility of in-flight aircraft. However, replacement is very costly and time consuming, due to the variety and number of existing aircraft and aircraft engines.

The second alternative can be effective. However, fuel additives are organo-metallic compounds (e.g., Ferrocene), which deposi_metallic oxides on engine surfaces. Considering the cost of the engine and its maintenance, and the cost of the aircraft, anything that may permanently alter engine parts is considered highly undesirable.

The third alternative does not affect the engine. Because of this, it is the only alternative which state regulatory authorities can impose. Nevertheless, particulate control

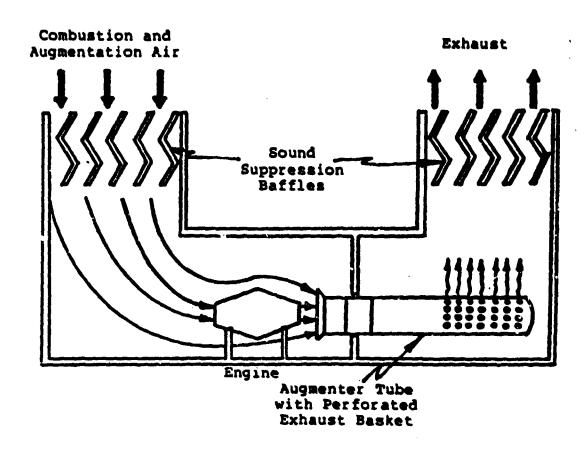


Figure 1. Generalized Test Cell Schematic

devices cannot be designed to meet an opacity requirement, only a specified degree of particulate removal.

The purpose of this study was to establish the connection between test cell particulate emissions and plume visibility as a basis for specifying control devices that could be mounted on the test cell exhaust stack. In addition, theoretical calculations were made to see under what conditions electrostatic precipitators or venturi scrubbers might satisfy opacity regulations.

SECTION II

SMOKE NUMBER

Much data on jet engine particulate emissions are in the form of SAE smoke numbers (SN), which measure the relative contrast of a standard filter paper exposed to the exhaust emissions for a standard period of time. A few investigators (References 2-6) have taken simultaneous measurements of particle loading ("soot density") and smoke number. Fewer studies (References 6-8) have determined plume opacity as a function of smoke number. These data, which are generally of poor quality, are plotted in Figures 2 and 3 for various engines.

Also presented in Figures 2 and 3 arc empirical correlations based on Reference 9. The correlation in Figure 3 includes the results of Connor and Hodkinson's work (References 10, 11) relating observed visibility to plume transmittance.

As can be seen, there is about as much error in predicting the Ringelmann number directly from the smoke number, as there is in predicting mass loading. However, in order to determine opacity from loading, the particle size distribution must be known (involving an additional error), and a computer program used to make the calculation. In either case, the use of smoke numbers is a very unreliable tool in predicting test cell plume opacity.

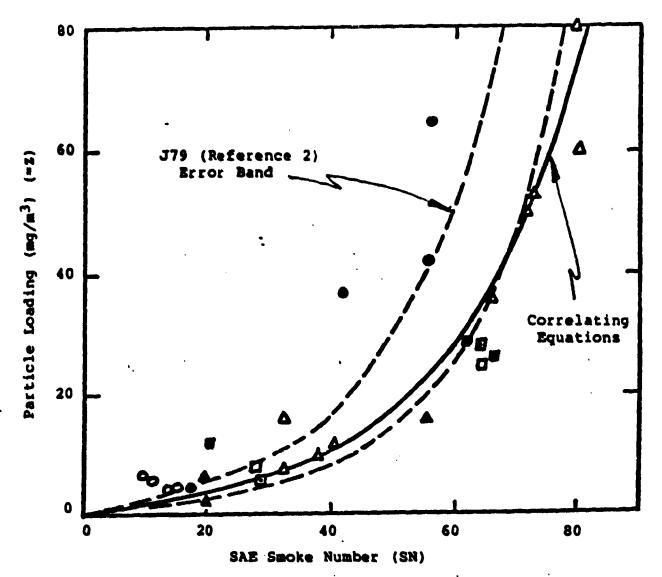


Figure 2. Relationship Between SAE Smoke Number and Soot Density (Reference 6)

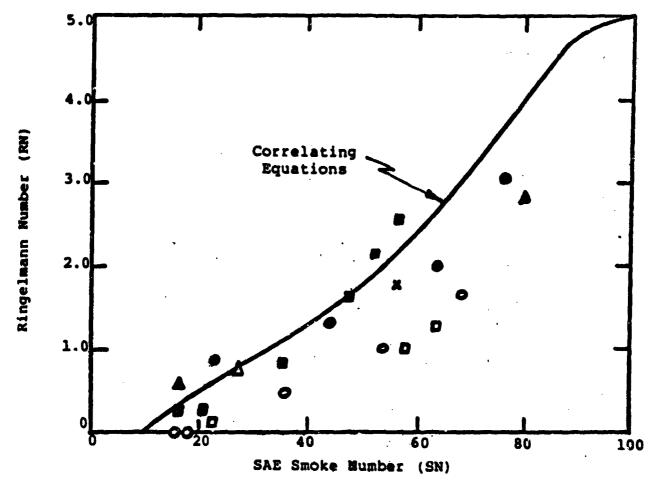


Figure 3. SAE Smoke Number vs. Ringelmann Reading (Reference 6)

Correlating Equations:

SECTION III

VISIBILITY EQUATIONS

Jet engine exhaust emissions largely consist of fine particles of unburned carbon. Because they are black, and therefore absorb much of the incident light intensity, carbon particles will exhibit very little back-scattering of ambient light. The visibility of black plumes is almost entirely a function of the relative contrast between the background sky-light and the amount of such light transmitted through the plume (Figure 4). This relative contrast is independent of observer position and can be calculated by the following equation (Reference 11):

$$T = \frac{B_T}{B_O} = \exp \left[\left(\frac{-3WD}{2\rho p} \right) \frac{1}{I} \sum_{i} \left(\frac{Q_{ext}}{dp} \right)_i \right]$$

where: T = transmittance, or relative plume brightness

 B_{T} = brightness of light transmitted through the plume

 B_0 = background sky brightness

W = particle loading

D = plume diameter

P_D = particle density

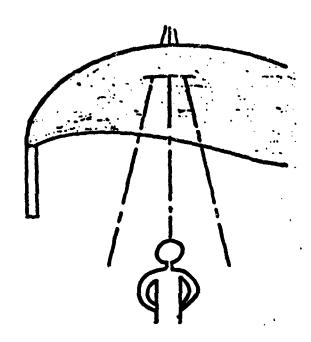
I = total number of particle sizes

dp = particle size

Qext = extinction coefficient, or ability of a given
particle to reduce the intensity of the transmitted light

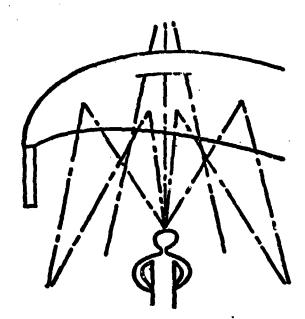
subscript i = 1th particle size in the distribution

The extinction crefficient for any given particle is determined by the following equation (References 11 and 12):



Black Plumes

For transmitted light, the observer sees only relative contrast with background sky brightness.



White Plumes

Scattered light originates from both in front and behind the observer. Therefore, the relative position of the sun is significant.

Figure 4. Visibility

$$Q_{\text{ext}} = \frac{2}{x^2} \sum_{n} (2n + 1) \text{Real}(a_n + b_n)$$

where: $x = \pi d_D/\lambda$

wavelength of light in which the plume is viewed (the computer program allows this value to be input, or if left blank assumes an average value for skylight of 0.550 microns)

a_n & b_n are complex Riccati-Bessel function of order "n":

$$\mathbf{a}_{U} = \frac{\phi_{U_{\bullet}}(\lambda) \, \delta^{U}(\mathbf{x}) - \mathbf{m}_{h}(\lambda) \, \delta^{U}(\mathbf{x})}{\phi^{U_{\bullet}}(\lambda) \, \delta^{U}(\mathbf{x}) - \mathbf{m}_{h}(\lambda) \, \delta^{U}(\lambda)}$$

$$b_{n} = \frac{m\psi_{n}'(y)\psi_{n}(x) - \psi_{n}(y)\psi_{n}'(x)}{m\psi_{n}'(y)\xi_{n}(x) - \psi_{n}(y)\xi_{n}'(x)}$$

y = mx

m = complex refractive index. This is a function of the wavelength of light (λ) at which it is measured, and also the method of generating the soot particles. The computer program allows this value to be input, or if left blank assumes a value for amorphous carbon at 0.550 microns of: 1.96 - 0.66i (References 13, 14). (Note: Because the transmitted light is altered both in phase and magnitude, a vector is needed to express the effect of the particles. As in electrical engineering, a vector can be expressed as a complex number with real and imaginary paxts. This is the case for the particle refractive index.)

Since these equations involve series functions of complex numbers, their solution is not simple. Instabilities can easily arise (particularly with large values of x), which cause the extinction coefficient to oscillate wildly and even produce negative values. In order to generate stable functions, the

following method is used (References 12, 15):

$$P_{n}(z) = \frac{d[\ln \psi_{n}(z)]}{dz} = \frac{\psi_{n}'(z)}{\psi_{n}(z)}$$

$$Q_{n}(z) = \frac{d[\ln \xi_{n}(z)]}{dz} = \frac{\xi_{n}'(z)}{\xi_{n}(z)}$$

(where z = y or x)

Therefore: $a_n = \frac{\psi_n(x)}{\xi_n(x)} \left[\frac{P_n(y) - mP_n(x)}{P_n(y) - mQ_n(x)} \right]$

$$b_{n} = \frac{\Psi_{n}(x)}{\xi_{n}(x)} \left[\frac{mP_{n}(y) - P_{n}(x)}{mP_{n}(y) - Q_{n}(x)} \right]$$

$$\Psi_{n}(z) = \Psi_{n-1}(z) - \frac{n}{z} \Psi_{n}(z)$$

$$\xi_n'(x) = \xi_{n-1}(x) - \frac{n}{x} \xi_n'(x)$$

Therefore: $P_{n}(z) = \frac{\psi_{n-1}(z) - \frac{n}{z} \psi_{n}(z)}{\psi_{n}(z)} = \frac{\psi_{n-1}(z)}{\psi_{n}(z)} - \frac{n}{z}$

$$= \frac{J_{v-1}(z)}{J_{v}(z)} - \frac{(v-1/2)}{z}$$

where J = Bessel function

$$v - 1/2 = n$$

Using Lentz's continued fraction method (15):

$$\frac{J_{v_1-1}}{J_{v_2}} = \frac{|w_1|w_2, w_1||w_3, w_2, w_1|....}{|w_2||w_3, w_2|.....}$$

$$w_p = (-1)^{p+1} \frac{2(v+p-1)}{z}$$

$$|w_{p}, w_{p-1}, \dots, w_{1}| = w_{p} + \frac{1}{w_{p-1} + \frac{1}{w_{p-2} + \frac{1}{-1}}}$$

Convergence is reached for J_{V-1}/J_V when $|w_p,\ldots,w_1|$ in the numerator equals $|w_p,\ldots,w_2|$ in the denominator.

 $Q_n(x)$ is generated by the following recursion formula:

$$Q_{n}(x) = \frac{1}{\frac{n}{x} - Q_{n-1}(x)} - \frac{n}{x}$$
(where $Q_{0}(x) = -i$)

Since

$$\frac{\psi_{n-1}(x)}{\psi_n(x)} = \frac{Jv_{-1}(x)}{J_v(x)}$$

$$\Psi_{n}(x) = \Psi_{n-1}(x) \left[\frac{J_{v}(x)}{J_{v-1}(x)} \right]$$

(where $\psi_{O}(x) = \sin x$)

Finally,

$$\xi_n(x) = \psi_n(x) + i\beta_n(x)$$

$$\beta_n(x) = (\frac{2n-1}{x})\beta_{n-1}(x) - \beta_{n-2}(x)$$

(where
$$\beta_0(x) = \cos x$$
, and $\beta_1(x) = \frac{\cos x}{x} + \sin x$)

Following Wiscombe (Reference 12) the order (n) of these functions varies from 1 to N, where:

$$N = x + 4x^{1/3} + 2$$
, $x \ge 4200$
 $N = x + 4.05x^{1/3} + 2$, $8 \le x \le 4200$
 $N = x + 4x^{1/3} + 1$, $x \le 8$

These equations can be used to generate the requisite Riccati-Bessel functions, the extinction coefficient, and finally the transmittance.

Once the transmittance (T) is calculated, the Ringelmann number may be obtained from the empirical correlation of Connor and Hodkinson (References 10, 11), Figure 5.

A computer program was written to perform these calculations. The FORTRAN listing and sample runs are given in the Appendices.

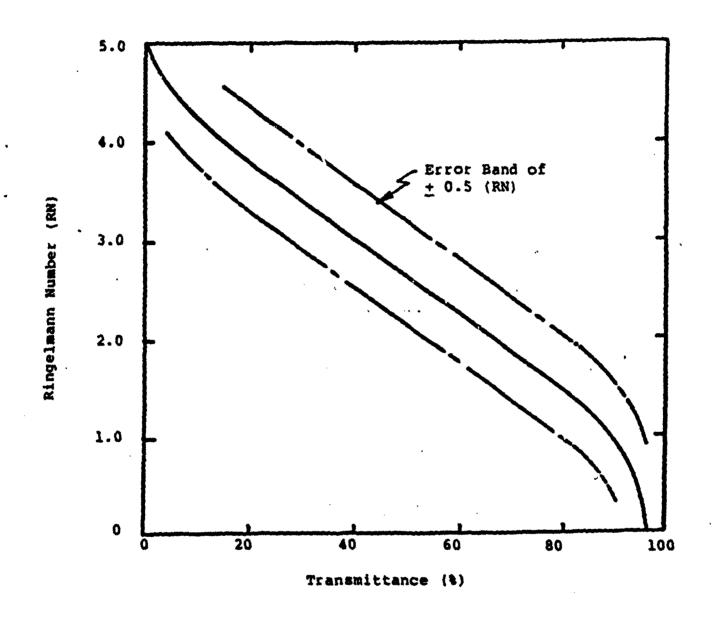


Figure 5. Black Plume Ringelmann Number Correlation with Transmittance (References 10, 11)

SECTION IV

ELECTROSTATIC PRECIPITATOR (ESP) EQUATIONS

A standard mathematical model (Reference 16) was used for predicting the ability of a wire-and-plate ESP to operate as a particle control device:

$$w_i = \frac{8.85 \times 10^{-5} E_c E_p d_{pi}}{\mu} (\frac{\xi}{\xi + 2})$$

$$n_i = 1 - \exp(\frac{-A_p w_i K}{Q})$$

 $\eta = \sum_{i} \eta_{i} m_{i}$

where: n = overall fractional collection efficiency

 η_i = fractional collection efficiency for particles of size d_{pi}

m_i = inlet mass fraction of particles of size d_{pi}

 A_p/Q = specific collection area of the ESP (A_p = total collection surface in m^2 ; and Q = gas flow in m^3/sec)

K = empirical constant

ξ = dielectric constant of the particles (dimensionless)

 μ = gas viscosity, in cp

E_C = electric field strength near the discharge electrodes, in kV/cm

Ep = electric field strength near the collecting
 plates, in kV/cm

 d_p = particles size, in microns

This model is based on a field-charging mechanism and is valid for particles larger than 0.5 microns.

If the collection efficiency for an ESP is plotted against the particle size, the resulting curve will exhibit a minimum in the range of 0.2 to 0.7 microns. Above that range, a field-charging mechanism predominates and the efficiency declines with particle size. Below that range, a diffusion-charging mechanism predominates and the efficiency increases with decreasing particle size. Since most of the particles emitted from a test cell are smaller than 0.2 μm , a large K value of 600 was used in order to compensate for the lack of a diffusion-charging mechanism in the model equations.

In order to reduce the amount of input data needed to run the computer program and avoid a prior design of the ESP, the following values were assumed:

 $\xi = 3$, for carbon

 μ = 0.024 cp, for air at 350°F and 1 atm

$$E_C = E_p = \frac{40 \text{ kV}}{(4.5 \text{ inches})(2.54 \text{ cm/inch})} = 3.50 \text{ kV/cm}$$

(where 9 inches is generally used as the plate-to-plate spacing in utility-type ESP's, with a secondary voltage of 40 kV).

The computer program takes the uncontrolled test cell emission data, calculates the fractional efficiencies, and then determines the outlet particle size distribution and loading. This information then goes to the visibility portion of the program where the outlet Ringelmann number is calculated.

SECTION V

SCRUBBER EQUATIONS

A standard mathematical model (Reference 17) was used to describe the particle collection efficiency of a high energy venturi scrubber. As with the ESP model, this also required an empirical factor (f) to make the model agree approximately with actual data:

$$\ln(1 - \eta_i) = -(\frac{18}{55}) \left(\frac{\rho l}{\rho_p}\right) \left(\frac{Q l}{Q_g}\right) \left(\frac{d_d}{dp_i}\right)^2 \frac{1}{C_i} \left\{ (k_i f + 0.7) - 1.4 \ln \left(\frac{k_i f + 0.7}{0.7}\right) - \left(\frac{0.49}{k_i f + 0.7}\right) \right\}$$

This equation is written in dimensionless form, and therefore any consistent set of units may be used:

 n_i = fractional collection efficiency for particles of size d_{pi}

Pr = liquid density

Pp = particle density

QL = liquid flow rate

 Q_g = gas flow rate

 C_i = Cunningham correction factor for gas viscosity; for particles that are the same size or smaller than the mean free path of the gas molecules (λ)

= 1 + $\frac{2 \lambda}{dp_i}$ [1.23 + 0.41 exp $\frac{-0.44 \ dp_i}{\lambda}$] (dimensionless)

 k_i = Stokes' parameter = $\frac{C_i \rho_p d_{p_i}}{9 \mu_0 d_d}$ Vg_T (dimensionless)

f ~ 0.5 (dimensionless empirical factor based on the author's experience) $Vg_{T} = gas velocity in the venturi throat <math display="block">= \sqrt{\frac{\Delta P_{T}}{\rho_{L}}} \frac{Q_{q}}{Q_{L}} g_{c}$

 ΔP_T = pressure drop across the venturi throat

gc = Newton's Law conversion factor

The following equations require specific units:

dd = mean drop size in the venturi throat (Reference 18), in microns

$$= \frac{1920}{V_{g_T}} \sqrt{\frac{\sigma_{\ell}}{\rho_{\ell}}} + 3.69 \left(\frac{\mu_{\ell}}{\sqrt{\sigma_{\ell}\rho_{\ell}}}\right)^{0.45} \left(\frac{1000 Q_{\ell}}{Q_{g}}\right)^{1.5}$$

og = surface tension of scrubbing liquid, in dynes/cm

 P_{ξ} = density of scrubbing liquid, in g/cc

με = viscosity of scrubbing liquid, in cp

Q₁ = flow rate of scrubbing liquid, in gpm

Qq = gas flow rate, in cfm

VgT in ft/sec

 λ = mean free path of gas molecules, in microns

 $= \frac{3.78 \, \mu_{\rm g}}{\sqrt{4 \, P_{\rm g} \rho_{\rm g}}}$

 μ_{Q} = gas viscosity, in cp

 P_q = gas pressure, in psia

 p_{α} = gas density, in lbm/ft³

Again, in order to minimize the input data requirements, the following operating conditions were assumed:

- (1) water is the scrubbing liquid at 70°F
- (2) gas properties are those of air at 350°F and 1 atm pressure.

For venturi scrubbers, QL/Qg (the liquid-to-gas ratio) is generally 5 to 30 gpm/l000 cfm, and ΔP_T is 10 to 70 inches of water.

The computer program takes the uncontrolled test cell emission data, calculates the fractional efficiencies, and then determines the outlet particle size distribution and loading. This information then goes to the visibility portion of the program where the outlet Ringelmann number is calculated.

As with electrostatic precipitators, the primary collection mechanism for venturi scrubbers should theoretically change in the range 1.0 to 0.1 µm. Above 1 µm, the particles are collected by an inertial mechanism, while below 0.1 µm a diffusional mechanism should prevail. Again, this would imply a trough in the fractional efficiency curve for particles in the 1.0 to 0.1 μm range. However, in practice, the collection efficiency of venturi scrubbers continues to decline below 0.1 μ m, indicating that the predominant mechanism remains This means that standard venturi scrubbers are inherently less efficient than ESP's in collecting particles smaller than 0.5 µm. One method of overcoming this deficiency has been to induce condensation in the gas stream, either before the scrubber (by quenching), or afterward (by utilizing a twophase ejector). However, these methods cannot as yet be mathematically modelled with any confidence and have not been included in the computer program.

SECTION VI

RESULTS & DISCUSSION

Grems (Reference 19) measured the particle size distribution, loading, and transmittance from a test cell at Mc-Clellan Air Force Base. However, the particle density was unknown. In the present study, this density was used as an empirical parameter to fit the computer results to Grems' data. Excellent agreement was obtained for a particle density of 0.92 g/cc (Table 1). For comparison, computer results are also shown for A particle density of 1.0 g/cc.

Soot particles are porous spheres of carbon, having a high void fraction. Solid carbon has a density of 1.8 to 2.1 g/cc. Therefore, a particle density of 0.92 g/cc implies a void fraction of about 0.53.

Although Grems' data indicated a bimodal particle size distribution, a straight-line log-normal fit was made by the computer program (see Figure 6).

Table 2 shows computer predictions of plume visibility when an electrostatic precipitator or venturi scrubber is used. For the ESP, a specific collection surface of $3281/m^2$ per 1000 m³/min of gas $(1000 \text{ ft}^2/1000 \text{ cfm})$ corresponds to an upper limit in commercial applications. Since the gas flow from a test cell is on the order of 200,000 scfm, $200,000 \text{ ft}^2$ of collecting plate would be required. However, even such a large ESP has only a small effect on the Ringelmann number because of the small particle size. The size range which has the greatest effect on visibility matches the wavelength of visible light—i.e., 0.2 to 0.7 microns. This is precisely the range in which an ESP or any other control device, is least efficient. Therefore, purchase of an electrostatic precipitator larger than the test cell would only have a marginal effect on plume visibility during the few hours per week the test cell is in use.

Similarly, a venturi scrubber designed for the limit of its range of operability would also have a marginal effect on test cell plume visibility. At a liquid-to-qas ratio of 30 gpm/1000 cfm (4.01 m³/min water per 1000 m³/min gas) the scrubber would produce 6000 gpm of waste water for a typical installation; and at a pressure drop of 70 inches of water (131 mm mercury) a 2400 hp tail fan would be required. Under these conditions, the computer predicts an overall particle collection efficiency of 49% with a visibility improvement of 0.5

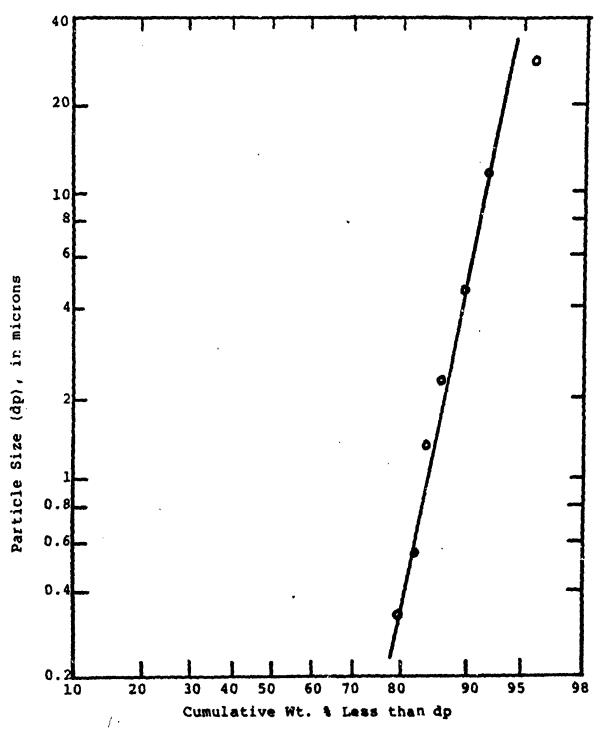


Figure 6. Log-Normal Plot of Size Distribution from Grems' Data (Reference 19)

TABLE 1. COMPARISON OF COMPUTER PREDICTIONS WITH GREEK' DATA FOR J57 ENGINE (Reference 19).

el Viring Rate (lbm/hr)	Particle Loading (mg/m ³)	Cum Wt 8	article Size Distributi Accodynamic Diameter* (-4p for pp-1.8 g/oc)	on Measured Transmittance	Predicted Transmittance (for p = 1.0 g/oc)	dp* (for pp 1 0.92 g/cc)	Predicted Transmittance (for pp = 0.92 g/cc
1000	2.16	93.5	23 🖪	961	88.31	24.0 m	87.41
		91.4	10.5		_	10.9	
		91.4	4		•	4.2	•
		87.A	2	•		2.1	
		84.9	1.1			1.15	
		79.9	0,57			0.59	
		73.5	0.33			0,34	
2500	1.95	95.7	20 11.5		89.4	29.2	22.6
		92.1	11.5	•		12.0	
		89.7	4.5			4.69	
		96.6	3.2			2.29	
		84.5 82.7	1.3 0.54			1.36 . 0.56	
		79.3	0,33			0.34	
0620	6.00			***			
4674	4.04	38.6	22 9.3	66	67.9	22.9 9.70	65.6
		96.6 95.1 92.0	3.5			3.65	
		92.8	1.7			1.77	
		90.5	0.94			0.98	
		83.6	0.47		••	0.49	
		77.4	0.23			0.24	
8625	6.34	\$7.7	21	66	60.4	21.9	66.2
		97.7	3.4	**		3.80	
		97.4	3.5			3.65	
		95.8	1.7			1.77	
		94.8	0.92			0.96	
		94.2	0.46			0.48	
		88.2	9,22			0,23	

Net open exhaust area = 700 ft² (700 = 26.5 ft, or 0 meters); refractive index for amorphous carbon at 550 mm = 3.96-0.661

*For a cascade impactor, dp1\fop1 = dp2\fop2

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TABLE 2. COMPARISONS OF CONTROLLED AND UNCONTROLLED EMISSIONS.

UNCONTROLLED EMISSIONS: (Plume Width = 8 Meters)

Particle Loading (mg/m ³)	Particle Density (g/cc)	Particle Size (um)	Cum.Wt. Less Than	Transmittance (%)	Ringelmann Number
6.34	0.92	21.9	97.7	66.2	1.5-2.5
, , , , , , , , , , , , , , , , , , , ,		9.80	97.7		
		3.65	97.4		
•		1.77	95.8		
		0.96	94.8		
		0.48	94.2		
		0.23	88.2		

CONTROLLED EMISSIONS:

(1) with ESP: $SCA = 3281 \text{ m}^2 / 1000 \text{ m}^3/\text{min}$

Outlet Particle Loading (mg/m ³)	Collection Efficiency (%)	Transmittance (%)	Ringelmann Number
2.93	53.8	82.8	0.9-1.9

(2) with Venturi Scrubber: $L/G = 4.01 \text{ m}^3/\text{min water per } 1000 \text{ m}^3/\text{min Gas}$ $\Delta P = 131 \text{ mm Bg}$

Outlet Particle	Collection	Transmittance (%)	Ringelmann	
Loading (mg/m ³)	Efficiency (%)		Number	
3.26	48.6	81.0	1.0-2.0	

Ringelmann number. Operating data with a scrubber (not a venturi) at the Jacksonville Naval Air Station (Reference 20) indicate an average particle collection efficiency of about 75%. However, there was considerable uncertainty in the accuracy of the data. Stockham, et al. (Reference 21) also report an average collection efficiency of 48% with water injection into the augmentor tube. Again, this is not venturi scrubber data, but it does indicate the validity of the order of magnitude of the predicted results. It should be noted that opacity measurement with a scrubber operating is virtually impossible, since the scrubber will emit a large and obscuring steam plume of its own.

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APPENDIX A

COMPUTER INPUT DATA FORMAT

The following pages give the format for the input data needed to run the computer program. The particle loading should be determined by EPA Method 5, and the particle size distribution by cascade impactor (Reference 19). The plume width can be approximated by the square root of the net open stack area (the actual stack cross-section minus the area occupied by acoustical baffles). For soot particles, the refractive index is 1.96-0.66i at a wavelength of 550 nm, and the particle density was estimated empirically as 0.92 g/cc.

Examples are given for:

- (1) Grems' data (19)
- (2) an electrostatic precipitator with a specific collection area of 1000 ft $^2/1000$ cfm (3281 m 2 of collecting plate per 1000 m $^3/min$ of gas)
- (3) a venturi scrubber with a liquid-to-gas ratio of 30 gpm/1000 cfm (4.01 m 3 /min of water per 1000 m 3 /min of gas) at a pressure drop of 70 inches of water (131 mm Hg).

CARD #1

This card contains the title of the case being run, inserted between columns 9 and 10.

CARD #2

This card contains the number of data pairs in the particle size distribution. The minimum number is 2, and the maximum is 100, inserted as an integer between columns 11 and 15 (right justified).

CARD #3 a, b, c, etc.

This card(s) contains the data pairs for the particle size distribution. Columns 1-10, 21-30, 41-50, and 61-70 contain values of the cumulative weight percent less than solvicle size d_p ; while columns 11-20, 31-40, 51-60, and 71-80 co tain the corresponding values of d_p . Therefore, a maximum of four data pairs can fit on one card. If there are more data pairs (as per CARD #2), these are put on subsequent cards, until the tal number of data pairs (cumulative weight percent less than d_p , and d_p) is equal to the number specified in CARD #2. All values are floating point numbers, with four digits (or blanks) to the right of the decimal point (right justified).

CARD #4

This card contains the following physical parameters: columns 11-15--the effective stack diameter in meters (based on the net open area) expressed as a floating point number, with two digits (or blanks) to the right of the decimal point (right justified)

- columns 16-22--the particle loading in mg/m³, as a floating point number, with two digits (or blanks) to the
 right of the decimal point (right justified)
- columns 23-28--the particle density in g/cm³, as a floating point number, with two digits (or blanks) to the
 right of the decimal point (right justified)
- columns 29-46--the particle refractive index. Columns 29-37 contain the real part, and 38-46 the imaginary part; both as floating point numbers with two digits (or blanks) to the right of the decimal point (right justified). If these columns are left completely blank, a value for amorphous carbon of 1.96-0.66i is assumed by the program. Note that the refractive index and the wavelength that follows must be consistent
- columns 47-53--the wavelength of light (in microns) at which the refractive index was measured, and at which the plume is presumed to be viewed. This must be expressed as a floating point number with three digits (or blanks) to the right of the decimal point (right justified). If columns 29-46 were left blank, these columns should also be left completely blank, in which case the program assumes a value of 0.550 microns.

CARD #5

This card contains (in column 2) an integer number which

indicates whether or not a particulate control device (electrostatic precipitator or venturi scrubber) has been installed on the test cell exhaust:

zero (0) means no control device

1 means an electrostatic precipitator

2 means a venturi scrubber

These are the only permissible cases.

CARD #6

This card depends on the code given in CARD #5.

- (a) If there is no control device (0 in column 2 of CARD\$5), CARD \$6 does not exist.
- (b) If an electrostatic precipitator is indicated by CARD #5, CARD #6 must contain the specific collection area (in m² of plate area per 1000 m³/min of exhaust gas) in columns 11-17 as a floating point number with one digit (or blank) to the right of the decimal point (right justified).
- (c) If a venturi scrubber is indicated by CARD \$5, CARD \$6 must contain the liquid-to-gas ratio (in m³/min water per 1000 m³/min exhaust gas) in columns 11-15; and the scrubber pressure drop (in mm mercury) in columns 16-23; both expressed as floating point numbers, with two digits (or blanks) to the right of the decimal point (right justified).

CARD #7

This card contains (in column 2) a code which tells the computer if more cases are to follow:

zero (0) signifies no more cases

I means an additional case follows

For each additional case, CARDS \$1 to 7 must be repeated, even if some of the data remain the same.

Figure A-1. Computer Input Data Format

Figure A-1. Continued. Computer Input Data Format

Figure 1-A. Continued. Computer Input Data Format

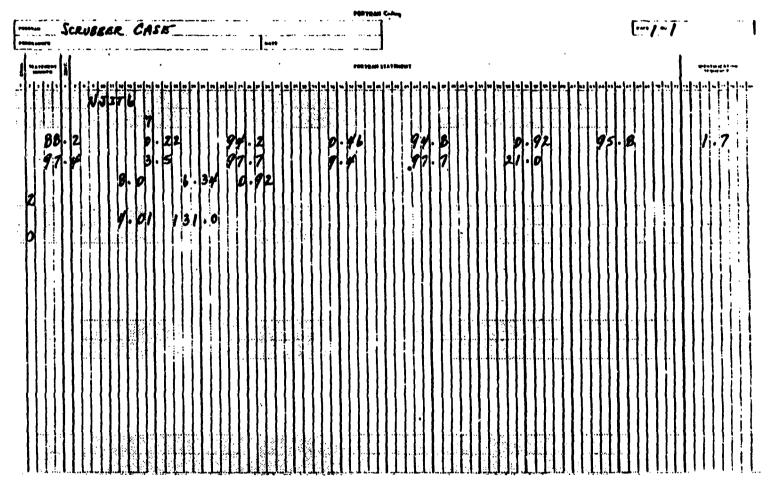


Figure A-1. Continued. Computer Input Data Format

APPENDIX B

OUTPUT FORMAT

Example outputs are given on the next few pages for the input data shown in the previous section (i.e. Grems' data, an ESP, and a venturi scrubber).

Figure B-1. Output Format

Figure B-1. Continued. Output Format

Figure B-1. Continued. Output Format

Figure B-1. Continued. Output Format

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Figure B-1. Continued, Output Format

Figure B-1. Continued. Output Format

Figure B-1. Continued. Output Format

Figure B-1. Continued. Output Format

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Figure B-1. Continued. Output Format

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Pigure B-1. Continued. Output Format

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Figure B-1. Continued. Output Format

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Figure B-1. Continued. Output Format

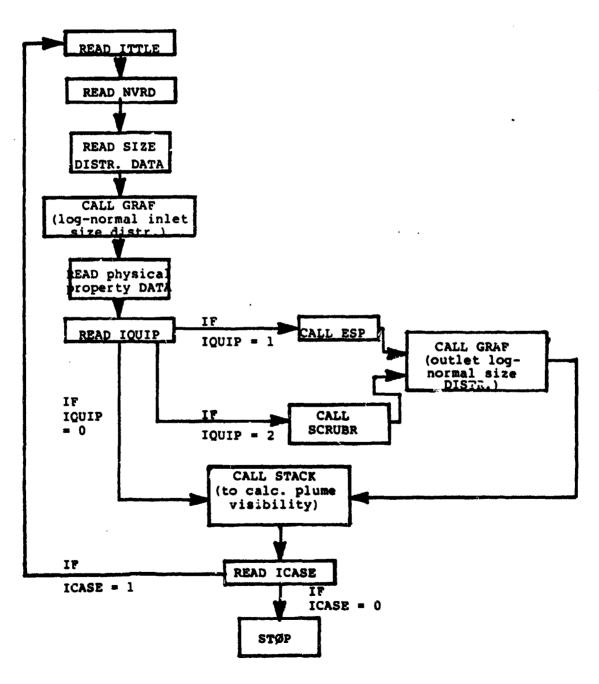
### APPENDIX C

## FORTRAN LISTING

The following FORTRAN program performs the various visibility and control calculations. It was originally written on a UNIVAC 90/80-3, and later converted for use on a CDC 6600. The version shown here is for the CDC 6600.

# COMPUTER PROGRAM FLOW CHART

Figure C-1.



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	C FROM AN ELECTRO-TATIC PRECIPITATE	ICLE SIZE DISTRIBUTION AND LOI ON MITH SPECIFIC COLLECTION SI	KUTRESSSSSSSSSSSSSSSSSSSSSSSSSSSSSSSSSSSS	
	COMMON/AESP/FF - SCA NE COMMON/AMORO/IN/RO, CLCV (101)		01025700	• •
10	C DIVENSION OF HALL-OPE HALL CHOEL	1011+SUME(101)	10026100	
	C FRACTIONAL EFFICIENCY = 1 = EXRI	SCAPPRIL	00026300 00026300	
15	C M = MIGMATION VELOCITY (M/SEC) = A	. MSE-05-EC-EP-DP-1CD/1CD-21)/	A 605990 A 605990	
	C EC = EP = FIFLD STHENGIN = 3.50 C UP = IM LT PARTICLE SIZE IN MICH	KY/CH HS	10026800	
>n	C FOR AIR AT 150 FF	ICULATES BATCH FOR CARRON IS	#800100627468 ##027166	
	C K . FUDRE FACTOM. SINCE THE MOD C MIGHATION VILOCITY APPLIES T	EL EQUATION FOR THE D PARTICLES LARGER THAM	99027366 9902740 <b>6</b>	
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	C FRACTIONAL EFFICIENCY = 1 - EXPL C WHERE SCA 18 IN M2 OF COLLECTING	9758-SCA-DP) -PLATE-PEN-1000_M3/M1M_GR_GAS	-FLOV0002000	
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	## ###################################	FRALL PALLECTION SPRIETRING A	<b>,,</b>	
<b>55</b>				
	17 PHOTOLOGY STREET PROTICE STR	<u> </u>		
68	Am115 (0.14)		9063[100	

Figure C-2. Continued. Computer Source Code Listing

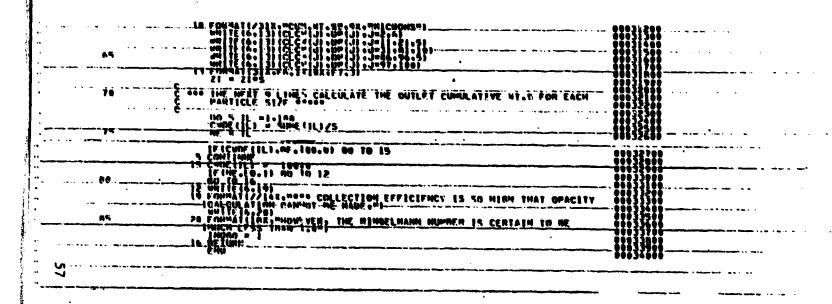


Figure C-2. Continued. Computer Source Code Listing

NF SCHURA 767175 0PT=1 FYM 4.81528	-30,267,261 - 13.62.18 ··· PAR
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C LOR(PT) = -   1/251 * RHOT / RHOT   ALGO   (DD/DP) * 2) * (1/CC) *	
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C RHOM = PANTICLE DEWSITY C ALR = LIQUID/GAS FLOW MATE	00035500 
C CC - CUMINGHAM CORRECTION FACTOR	91036999
C CAMAINA - "AS GEAN PREE PATH" - 67 1 57 MICHONS FOR AND AND I AIM	1 0036000 1 0036100
C VOT AS VISCOSITY . 9.00 CP FOR AIR AT 350 V AND 1 A	
C PD = P-ESSUME DRUP ACROSS THE SCHUBRER	
C FUR MATER AT 28 F1 V01 - 11.56-SORT (PD/ALO)	
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G) - (1001.0/907) · 20.07-(AL0-01.5)	
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Figure C-2. Continued. Computer Source Code Listing

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Figure C-2. Continued. Computer Source Code Listing

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<u></u>	<u> </u>	MARIMUM VALUES (MMAE) OF THE ORD FUNCTIONS ANY SCHERIED BY THE F ACCOMMING TO WILCOMPE WILL, APP 1804-1964 (988) COMPES	LIED OFFICS. VOL.19. PP.1505-	272177		_
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Figure C-2. Continued. Computer Source Code Listing

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	C PHY IS ANOTHER LOGARITHMIC DERIVATIVE FUNCTION. ALAZAS AND C USTATUS AND THE POSSIBILITY OF EXPONENTIAL C UNKNELLULAR COMPLEX MUMBERS.	{1133511
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	13 = HF VI (MA) - MELOCOMMIN (4) 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1	<b>3333733</b>
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	>4 18445 # EXP[[1-[3,6E-63]*Z[*PATH]/(200,0*RHOP)]*STEPS)	
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Figure C-2. Continued. Computer Source Code Listing

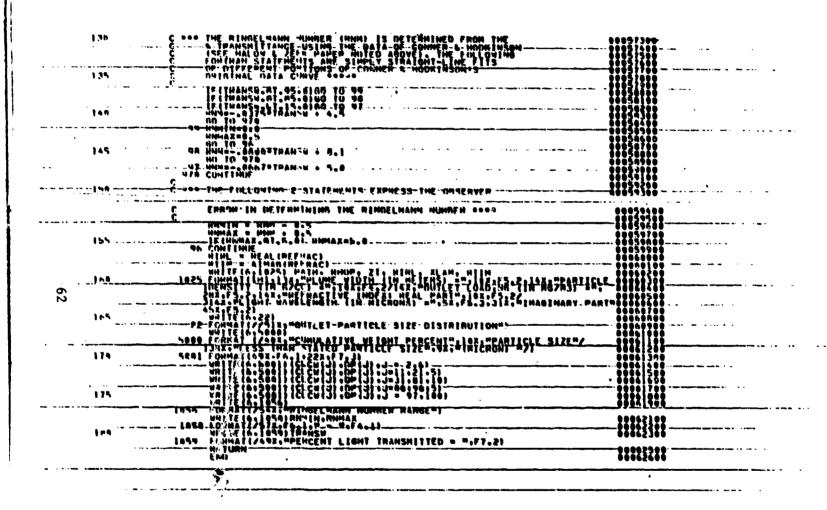


Figure C-2. Continued. Computer Source Code Listing

### APPENDIX D

#### COMPUTER PROGRAM NOMENCLATURE

Al real part of an denominator an numerator/Al A2 A3 an denominator/Al AN Stokes' parameter (k) in Calvert's scrubber equa-AK tions (dimensionless) AKF AK(f) + 0.7, where f = 0.5ALG liquid/gas ratio intercept of straight-line log-normal equation (in GRAF) BIMAG Bl real part of b_n denominator **B**2  $b_n$  numerator/Bl **B**3 b_n denominator/Bl BJ  $J_{V-1}/J_V$  (with real argument) BJC  $J_{V-1}/J_{V}$  (with complex argument) bn

BN

CC Cunningham correction factor in scrubber equations (dimensionless)

CLCW cum. wt. % in 1% increments

CN n/x

CMDE outlet cummulative wt. % from ESP

CWDS outlet cummulative wt. & from scrubber

**CWRD** raw cum. wt. % input data DD = scrubber drop size (by Nukiyama-Tanasawa equation), in microns

DHUN is defined by line 7 of function EINV

DPE = outlet particle size from ESP (in microns)

DPRD = raw particle size data (in microns)

DPS = outlet particle size from scrubber (in microns)

DPl = average value of DP in interval (microns)

EFF = calculated ESP efficiency (%)

EFFS = calculated scrubber efficiency (%)

EINV(RCW) = inverse normal distribution function (RCW = variable)

ETA is defined by line 17 of function EINV

ETASQ . is defined by line 16 of EINV

E3 = 1/3

EF2 is defined by line 15 of function EINV

FND = FLOAT (NVRD)

G is defined by line 37 of subroutine ESP

GRAF is a subroutine that uses the method of least squares to fit the raw particle size distribution data to a straight-line equation

I, IJ, IK, IL are all counters

ICASE = 0, when there are no further cases, and = 1 when
another set of data cards (i.e. another case)
follows

INOGO = 1 if the electrostatic precipitator, or scrubber, has such a high efficiency that virtually all of the original particle size distribution is collected. Otherwise, it is 0.

IP = p (in generating values of w)

IQUIP = 0, if there is no particle collection device; = 1, if there is an electrostatic precipitator; = 2, if there is a venturi scrubber

ITTLE = alphanumeric variable (maximum of 10 letters) corresponding to the case title.

J,JI are counters

K = counter

L =  $(-1)^{p+1}$  (in generating values of w)

N = n (order of Riccati-Bessel functions)

NE = number of data pairs for outlet distribution from ESP

NMAX = max. value of n

NS = number of data pairs for outlet distribution from scrubber

NVRD = number of raw data pairs for inlet size distribution

PATH = plume width = effective stack diameter (in meters)

FD = pressure drop across scrubber (in mm. mercury)

 $PNX = P_n(x) = \psi_n'(x)/\psi_n(x)$ 

 $PNY = P_n(y) = \psi_n(y)/\psi_n(y)$ 

PTLN = natural log of scrubber penetration

 $Q = Q_n(x) = \xi_n'(x)/\xi_n(x)$ 

QEXT = extinction coefficient =  $\frac{2}{\sqrt{2}} \Sigma (2n+1) \operatorname{real}(a_n+b_n)$ 

QSUM =  $\Sigma(2n+1) \operatorname{real}(a_n+b_n)$ 

 $RB1X = \psi_n(x)$ 

RB2 =  $\beta_n(x)$ 

RB3 =  $\xi_n(x)$ 

REFRAC = complex refractive index of particle (dimension-less)

RHOP = particle density (in g/cc)

RIIM = imaginary part of refractive index

RIRL = real part of refractive index

RNM = calculated Ringelmann number

RNMAX = upper estimate of Ringelmann number (=RNM+0.5)

RNMIN = lower estimate of RNM

s = fractional penetration

SCA = specific collection area of ESP (in m² per 1000 m³/min of gas)

SGN is defined by lines 11 and 14 of EINV

SLOPE = slope of straight-line log-normal equation (in GRAF)

STACK is the subroutine that calculates plume visibility

STEPB =  $\sum_{i} (\frac{Q_{ext}}{dp})_{i}$ 

SUM = % penetration

SUME = cumulative wt % penetration for particles of size DPE

SUMS = cumulative wt % penetration for particles of size DPS

SUMX - EX

SUMXY = EXY

SUMX2  $\Rightarrow \Sigma(X^2)$ 

SUMY = IY

TRANS = calculated fractional transmittance =  $\exp\left\{\left(\frac{-3WD}{2pp}\right)\frac{1}{100}\sum_{i=1}^{100}\left(\frac{Q_{ext}}{dp}\right)_{i}\right\}$ 

```
TRANSW
                transmittance
             gas velocity in venturi scrubber throat (in me-
VGT
            |wp,...,w2|, with real arguments
WD
             |wp,....,w2|, with complex arguments
WDC
             IMAG (WNC-WDC)
WI
             |wp,....,wl|, with real arguments
             |wp,....,w1|, with complex arguments
WNC
             w_p = (-1)^{p+1} \frac{2(v+p-1)}{x}
            (-1)^{p+1} \frac{2(v+p-1)}{y}
WPC
WR
             real (WNC-WDC)
             EINV (CWRD)
X
X1
             EINV (CLCW)
             x2
X2
XLAM
             wavelength of light used to view the plume (\lambda) (in
             microns)
             #dp/λ (dimensionless)
             log10 DPRD
             m^{\dagger}dp/\lambda (dimensionless)
ZI
             particle loading (in mg/m^3)
```

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